



## **FGD Water Treatment R&D Summary**



ORSANCO

190<sup>th</sup> Technical Committee Meeting

Nashville, Tennessee

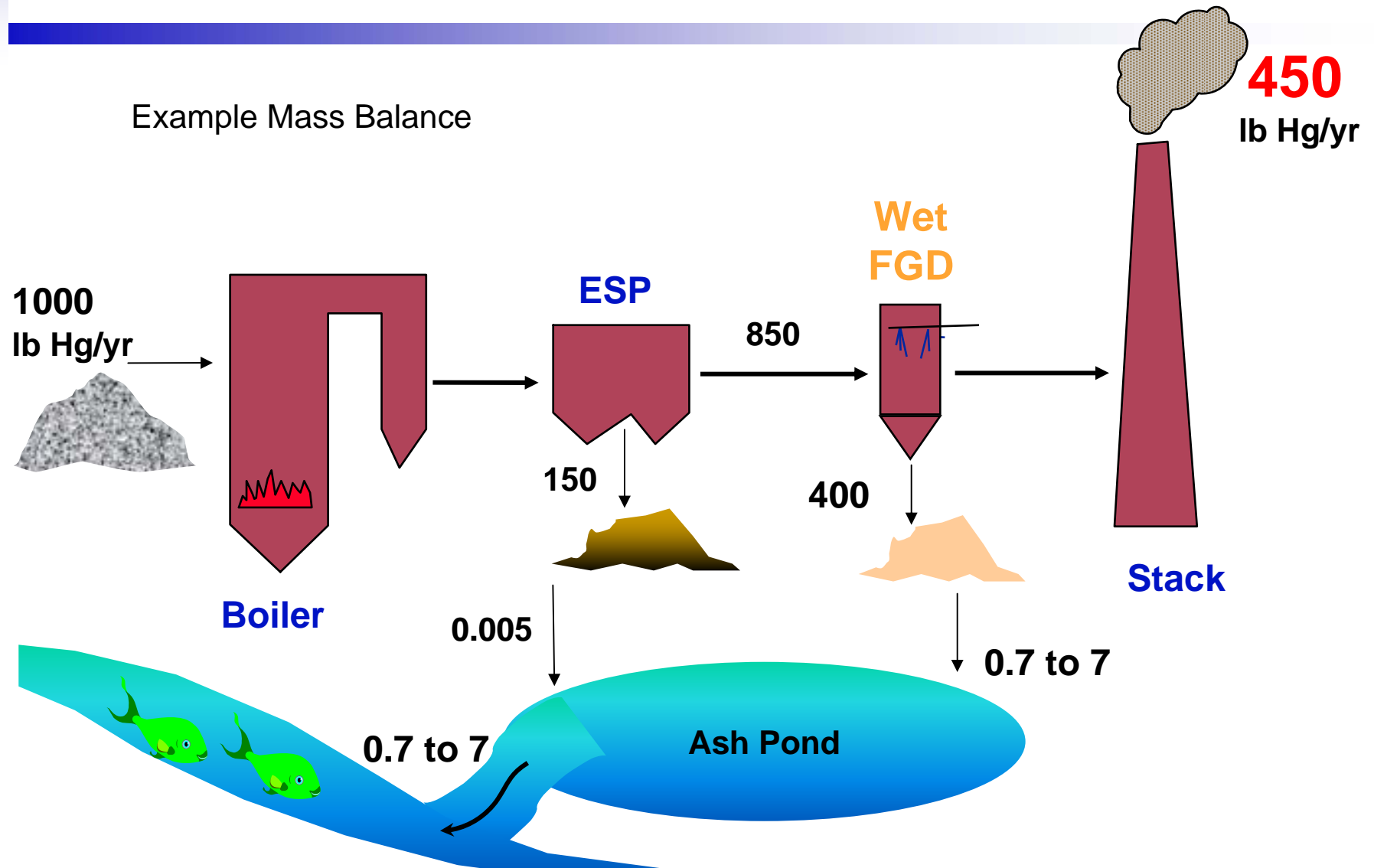
June 2, 2009

**Paul Chu, John Goodrich-Mahoney**

# Multimedia Fate of Mercury

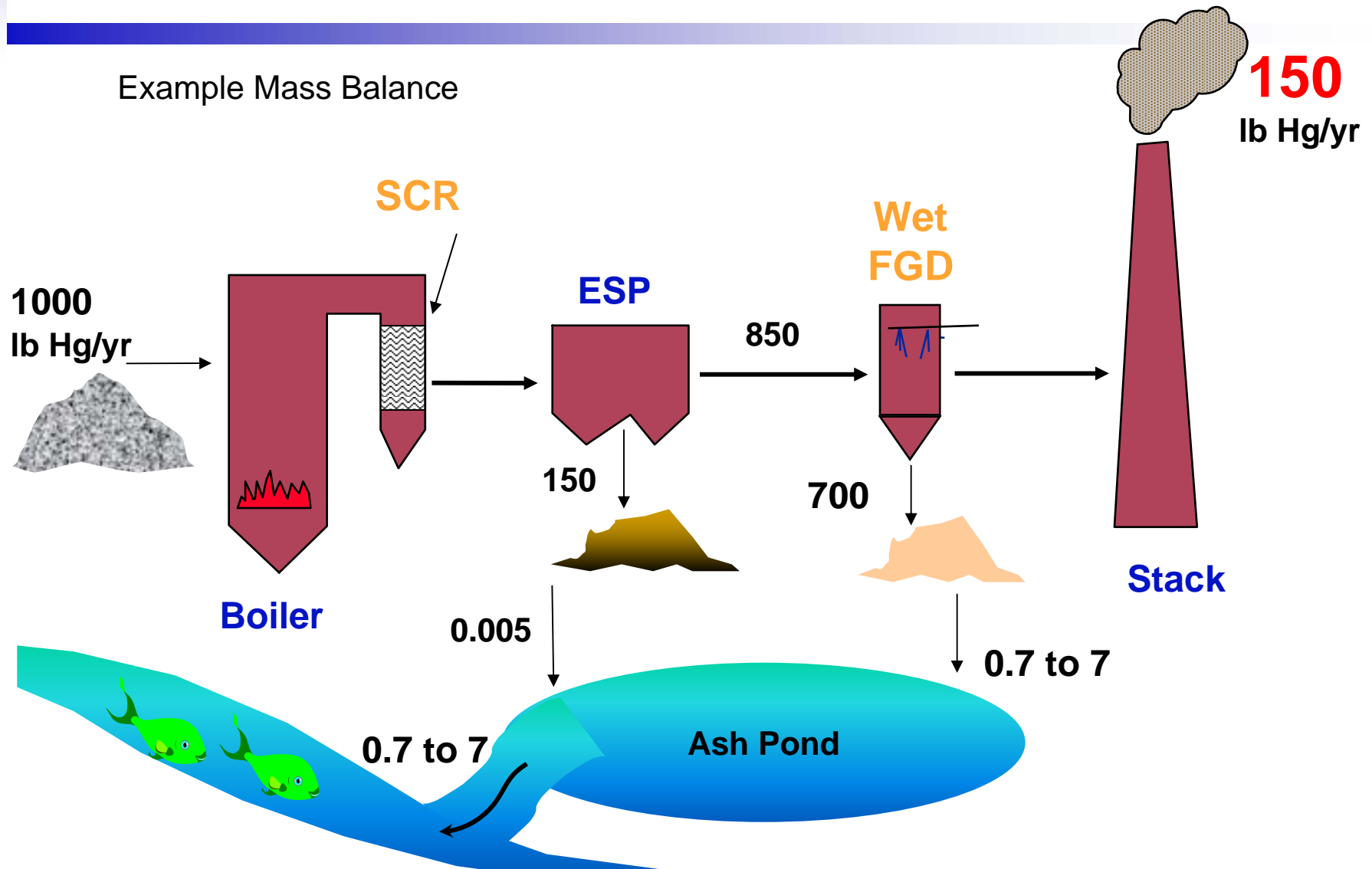
## *Baseline with FGD only*

Example Mass Balance



# Flue Gas Mercury Generally Captured with Combined SCR and FGD

Example Mass Balance



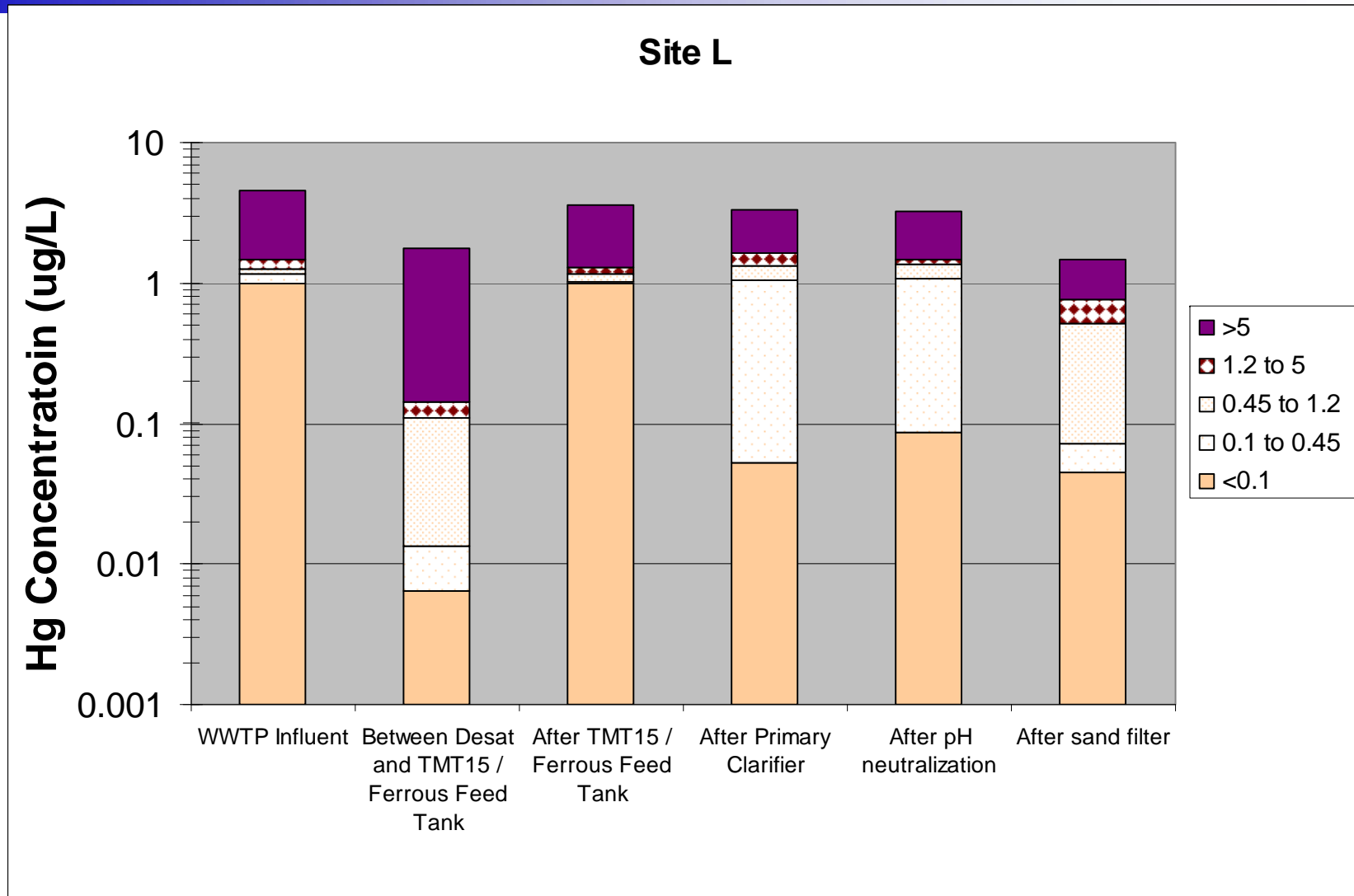
# Full-Scale FGD Water Treatment Technologies

*Installed/Operating at US Power Plants*

- Physical/Chemical
  - Iron coprecipitation (metals)
  - Organo-sulfide precipitation (mercury)
- Biological/wetlands (selenium, metals)
  - Polishing, downstream of physical/chemical system

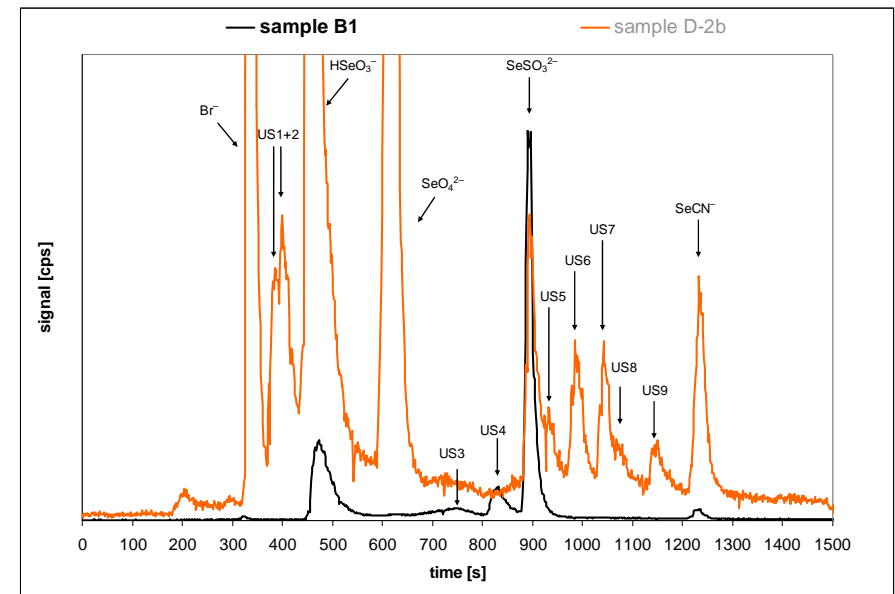


# Traditional Sulfide Precipitation: May Yield Submicron Particles *(Based on Limited Data)*

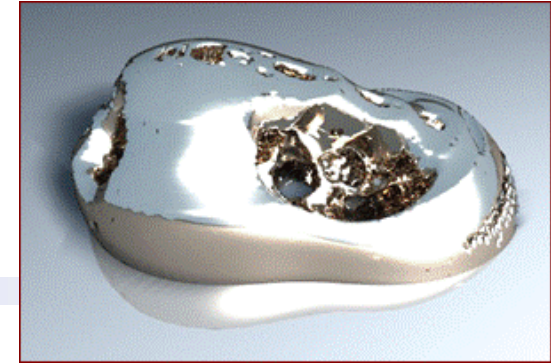


# Selenium May Be Present in Several Chemical Forms in FGD Waters

- Different treatment implications
- Selenite – Se(IV)
- Selenate – Se(VI)
  - Difficult to treat
- Elemental selenium – Se(0)
  - dissolved
  - colloidal
- Selenocyanate
- Selenosulfate –  $\text{SeSO}_3^{2-}$
- Unknown/unaccounted-for forms



# EPRI Treatment Project Objectives



- Independent, 3<sup>rd</sup> party evaluation
- Evaluate technologies:
  - Mercury (Hg): 1-10 ppt
  - Selenium (Se): 50-100 ppb, including all species

# '08 Pilot EPRI Water Treatment Studies

- Pilot studies: most promising technologies
  - Short-term feasibility evaluation
- Powder River Basin (PRB) site
  - Metallic Fe cementation (targeting selenium)
  - Fe/Sulfide + microfiltration
  - Two (2) adsorption approaches
- Eastern bituminous site
  - Vertical flow wetland (subsurface)
- Full-scale evaluation of GE ABMet biological reduction (eastern bituminous site)





# Metallic Iron Cementation Pilot (PRB site)

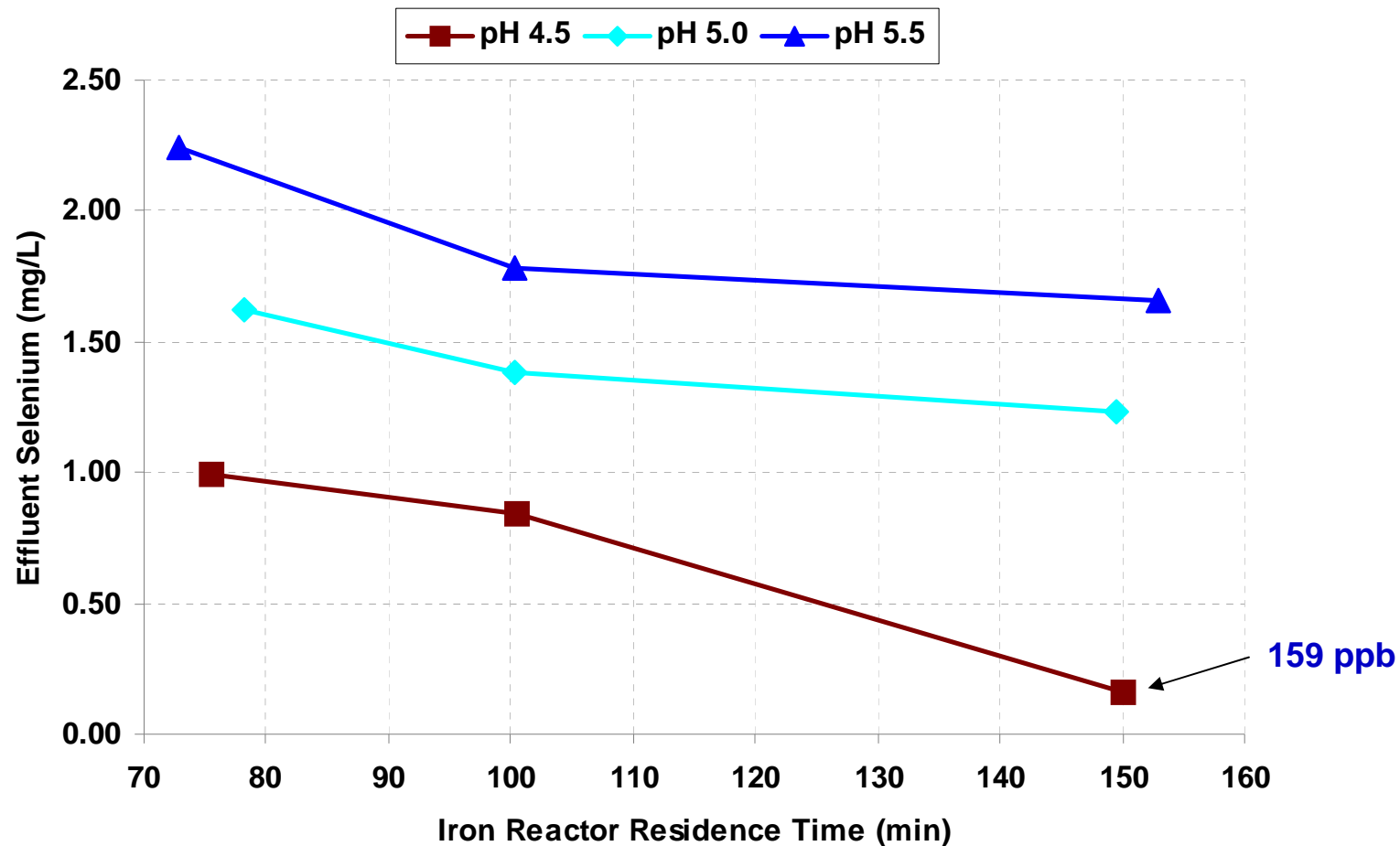
*Target: Selenium Removal*



# Metallic Iron Cementation: Se removal

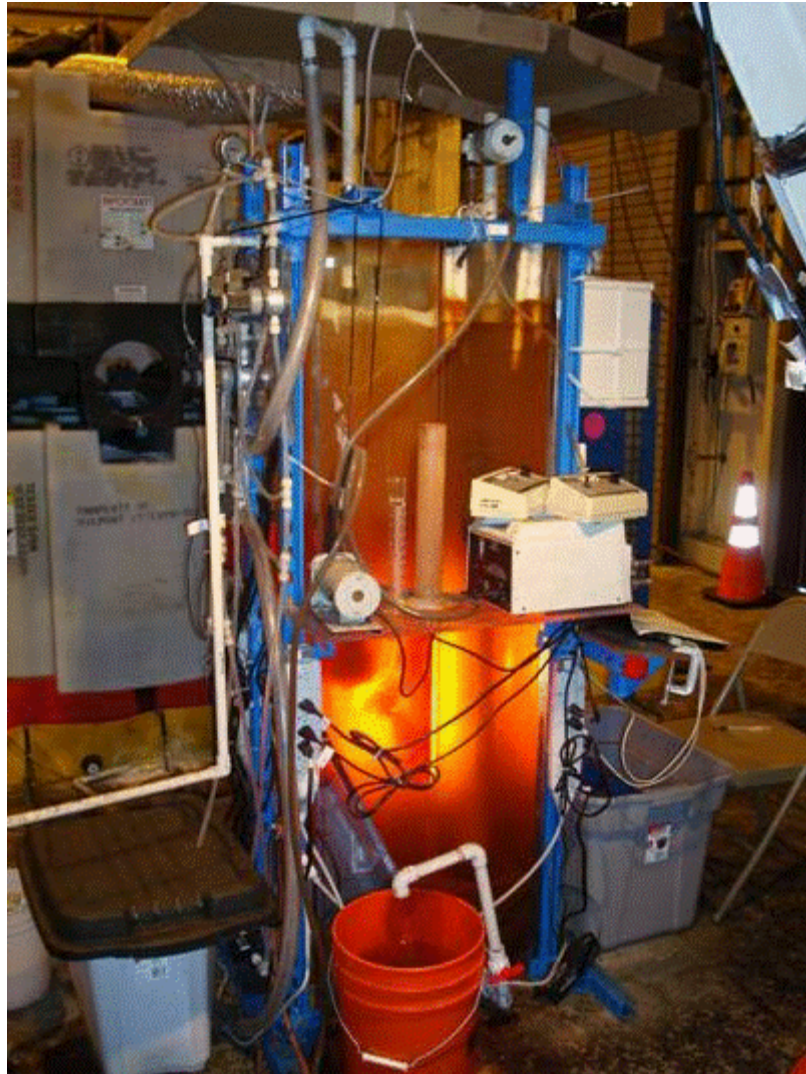
## *Need for More Residence Time, Lower pH*

- Influent ~6000 ppb dissolved Se; 2000 ppb  $\text{Se}^{+6}$



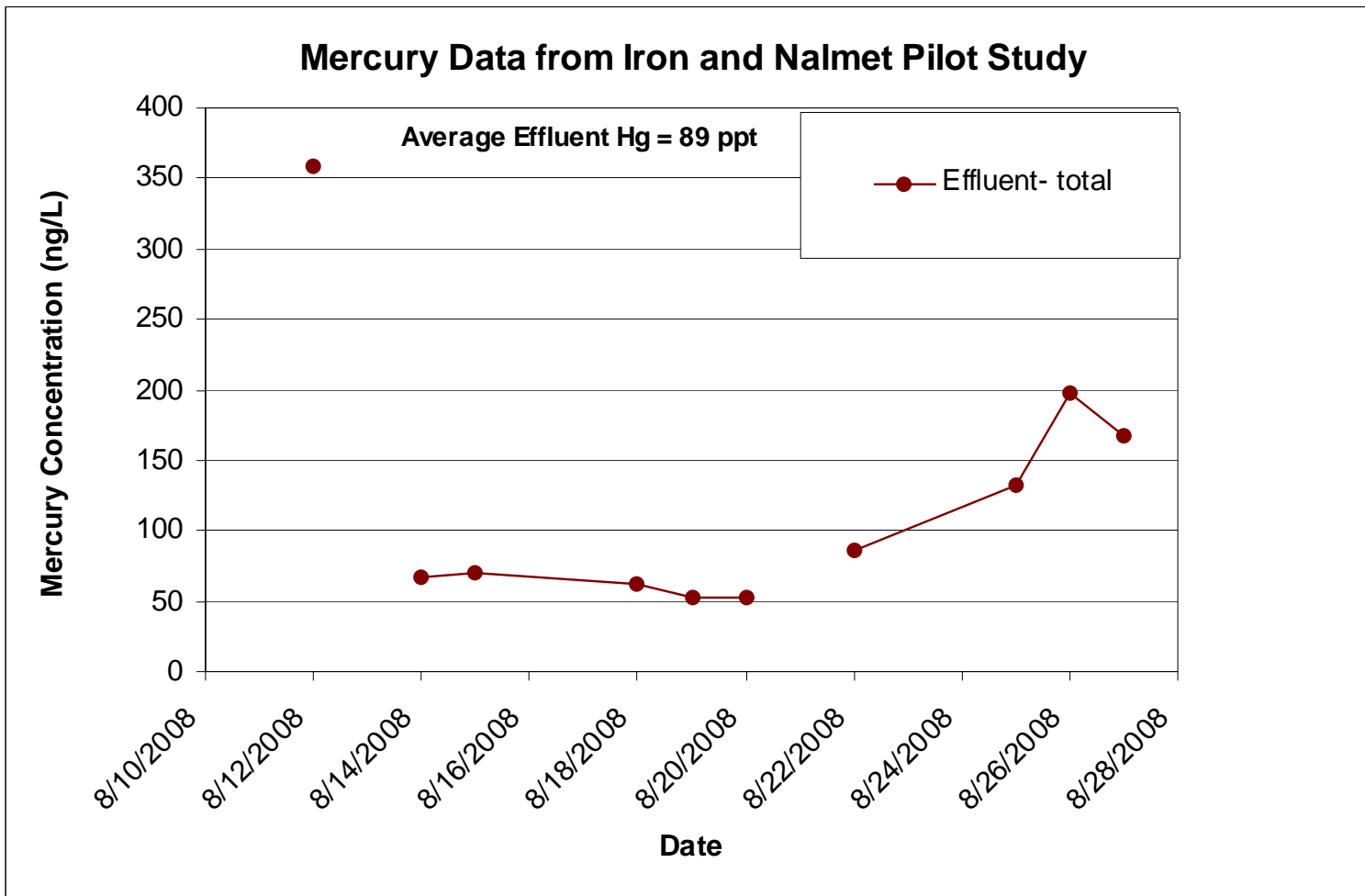


## Iron/Sulfide + Microfiltration Pilot (PRB site)



# Iron/Sulfide + Microfiltration

*Pilot results indicate modest Hg removal improvement*



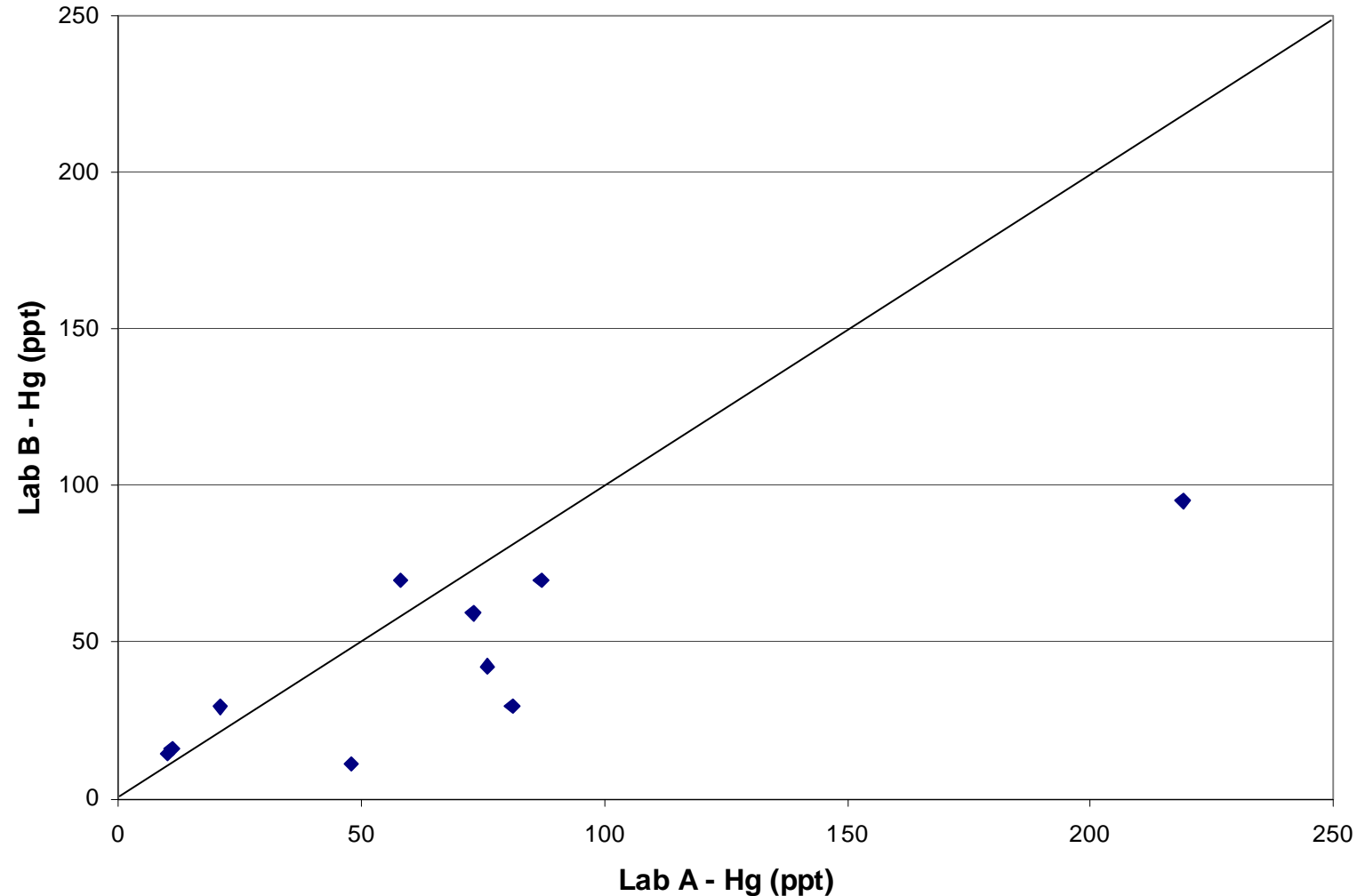


# Microfiltration followed with Adsorption Technology (PRB site)



# Microfiltration + Adsorption Draft Results

*<100 ppt possible; lab comparisons “just ok”*



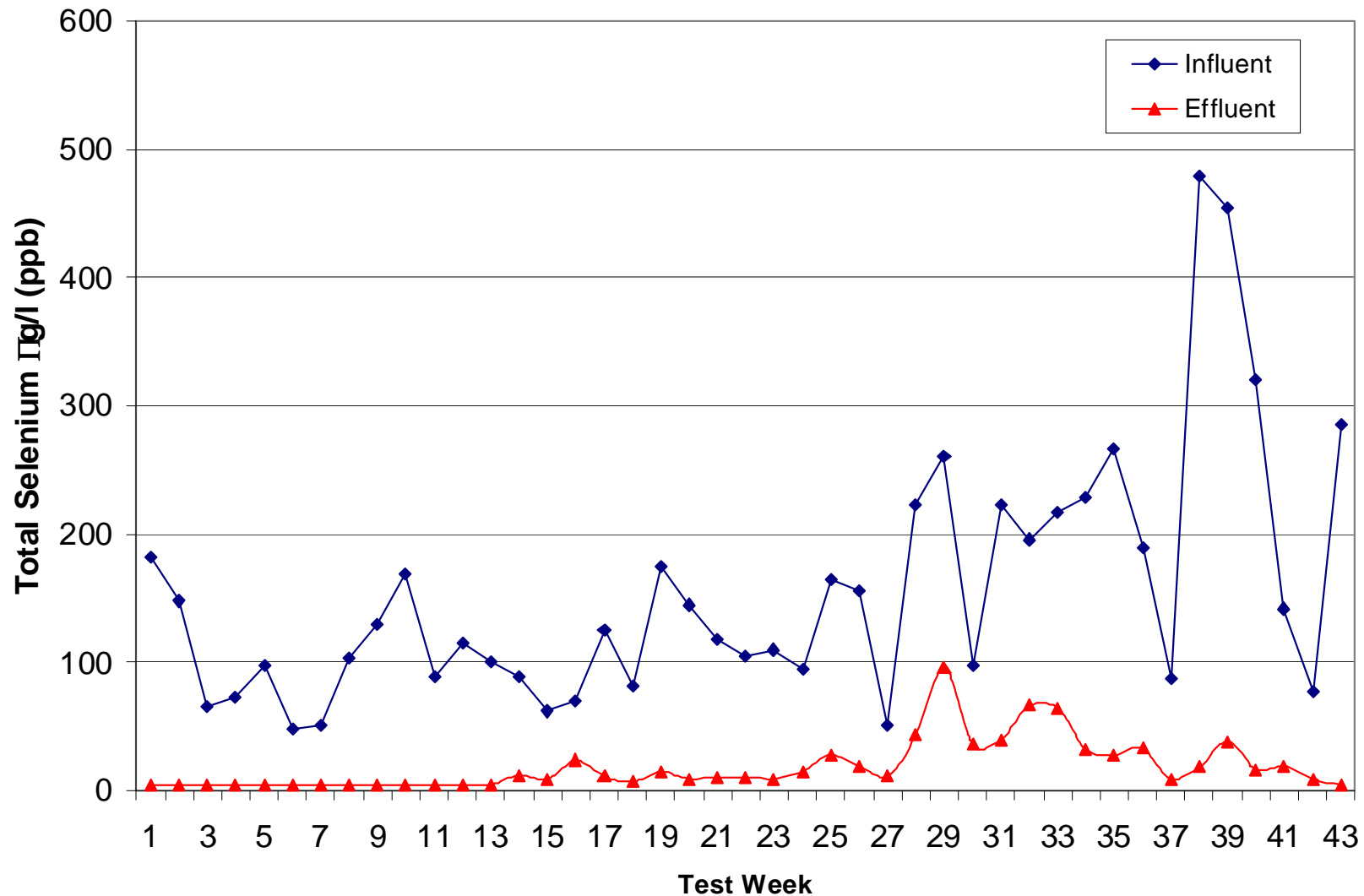
# Vertical Flow Wetland Pilot: Eastern Bituminous

## *Anaerobic, Reducing Wetland*



# Selenium Removals Appear Promising

*Note: Influent Se Levels are Low, Primarily Se<sup>+4</sup>*





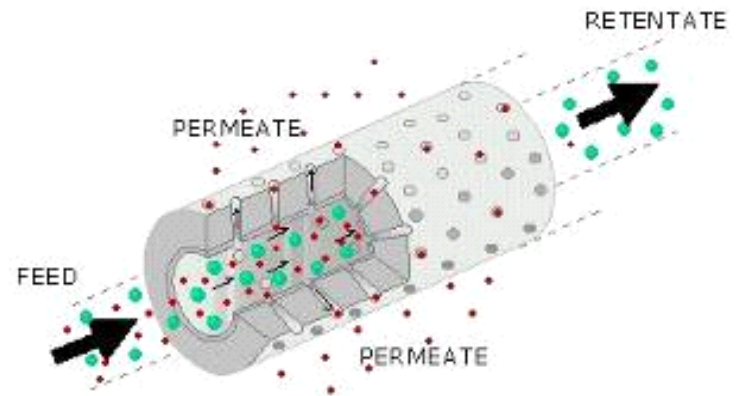
# GE ABMet Biological Evaluation



- Microbial reduction and precipitation of Se (and other metals)
- Sampling/analytical studies ongoing
- Much of the Hg and Se are being removed in the physical/chemical system upstream of the bioreactor
  - Inlet Hg/Se levels are very low, but are being successfully treated in the bioreactor
  - Primarily selenite ( $\text{Se}^{+4}$ ); but the selenate ( $\text{Se}^{+6}$ ) is being removed
- Speculate whether this FGD water matrix is easier to treat

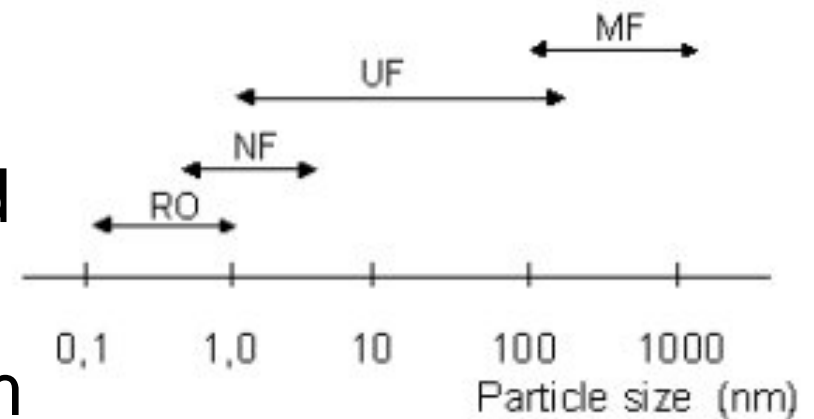
# Total Dissolved Solids (TDS) Water Treatment

- Possible treatment considerations
- Underground injection
  - Geology consideration
- Microfiltration/Ultrafiltration
- Evaporation
  - Ponds
  - Brine Concentrator/Crystallizer
  - Spray dryer



# Will Filtration Remove TDS?

- TDS are primarily salts
- Microfiltration (MF), ultrafiltration (UF) – several studies indicate little removal
- Reverse osmosis (RO) would remove TDS
  - Concentrated water stream to manage
  - Operability issues



# Evaporative Approaches



- Evaporation Ponds
  - More common, applicable in arid, western applications
- Reinjection into flue gas
  - Corrosion issues
  - Nozzle pluggage, solids deposition
  - Particulate emission increases (flue gas)
- Brine Concentrator + Crystallizer/spray dryer
  - “ZLD”: capital/operating costs are significant

# Brine Concentrator/Crystallizer



- Thermal evaporation
- Full-scale systems recently started up in Italy
  - KCPL Iatan system to come online in '09
- Generally consists of:
  - Salt conversion (with sodium)
  - Brine concentrator (to reduce water volume)
  - Crystallizer (produce solid waste)
- Capital costs likely several times greater than current physical/chemical water treatment
- Thermal energy requirements ~several % of plant load
- Solid wastes: unclear on leachability

# Summary



- Much ongoing work by EPRI and others
- Each power plant - somewhat unique in terms of coal, limestone/lime, power plant and FGD design
- Water treatment
  - Limited pilot screening data, generally 1 data point
  - Several promising technologies for Hg and/or Se
  - Achieving 1-10 ppt Hg ??
  - More data needed
- Believe/speculate that some water matrices are easier (or more difficult) to treat
- TDS: likely difficult, costly to treat